

(12) INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(19) World Intellectual Property Organization
International Bureau



(43) International Publication Date
27 June 2002 (27.06.2002)

PCT

(10) International Publication Number
WO 02/49442 A1

(51) International Patent Classification⁷: **A23C 1/04**,
21/00, A23L 1/24, A23J 1/08, 1/20, 3/04, 3/08, A23L
1/307

(21) International Application Number: PCT/GB01/05648

(22) International Filing Date:
19 December 2001 (19.12.2001)

(25) Filing Language: English

(26) Publication Language: English

(30) Priority Data:
0030926.0 19 December 2000 (19.12.2000) GB

(71) Applicant (for all designated States except US): **HERIOT-
WATT UNIVERSITY** [GB/GB]; Riccarton Campus, Ed-
inburgh EH14 4AS (GB).

(72) Inventor; and

(75) Inventor/Applicant (for US only): **CAMPBELL, Lydia,
Johanna** [ZA/GB]; 16 Victoria Avenue, Milnathort KY13
9YE (GB).

(74) Agents: **MCCALLUM, William, Potter** et al.; Cruik-
shank & Fairweather, 19 Royal Exchange Square, Glasgow
G1 3AE (GB).

(81) Designated States (*national*): AE, AG, AL, AM, AT, AU,
AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN, CO, CR, CU,
CZ, DE, DK, DM, DZ, EC, EE, ES, FI, GB, GD, GE, GH,
GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC,
LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW,
MX, MZ, NO, NZ, OM, PH, PL, PT, RO, RU, SD, SE, SG,
SI, SK, SL, TJ, TM, TN, TR, TT, TZ, UA, UG, US, UZ,
VN, YU, ZA, ZM, ZW.

(84) Designated States (*regional*): ARIPO patent (GH, GM,
KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZM, ZW),
Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM),
European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR,
GB, GR, IE, IT, LU, MC, NL, PT, SE, TR), OAPI patent
(BF, BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR,
NE, SN, TD, TG).

Published:

- with international search report
- before the expiration of the time limit for amending the
claims and to be republished in the event of receipt of
amendments

For two-letter codes and other abbreviations, refer to the "Guid-
ance Notes on Codes and Abbreviations" appearing at the begin-
ning of each regular issue of the PCT Gazette.

(54) Title: **FAT REPLACEMENT MATERIAL AND METHOD OF MANUFACTURE THEREOF**

(57) **Abstract:** The present invention provides a method for the manufacture of a fat replacement material suitable for use in the manufacture of food products. The method comprises the steps of: a) providing a substantially homogeneous aqueous fluid containing albumin and at least one stabilizer selected from a sugar and salt; b) subjecting the fluid to a controlled heat treatment at a temperature and for a period of time not less and not greater than that sufficient for obtaining from 50 to 100% denaturation of the albumin; and c) spray drying of the heat treated fluid. The invention also provides a fat replacement material comprising a spray dried powder comprising an intimate admixture of 1 part by weight of from 50 to 100 % denatured albumin, and from 3 to 100 parts by weight of at least one stabilizer selected from a sugar and salt. The material of the invention has excellent emulsifying properties as well as improved heat stability and resistance to acid conditions.

WO 02/49442 A1

-1-

FAT REPLACEMENT MATERIAL AND METHOD OF MANUFACTURE THEREOF

The present invention relates to the manufacture of a fat replacement material suitable for use in the food industry.

5 It has previously been proposed to use albumin proteins such as whey and egg white to substitute for fat to a greater or lesser extent so as to produce low-fat food products for which there is an ever increasing demand. It is however particularly important for safety reasons, when using albumin
10 to ensure that it is properly pasteurized. When albumin is subjected to heat treatment, though, there is a considerable risk of the albumin coagulating and/or being hydrolyzed, which generally results in processing difficulties and adverse effects on the texture, mouth-feel, and other properties of
15 the final food product in which it is used. Conventionally therefore manufacturers have gone to considerable lengths to avoid any denaturation of the albumin as far as possible in order to prevent the albumin from coagulating.

20 Whey is generally defined as the liquid byproduct from the manufacture of cheese and casein by the acid or rennet coagulation of milk. The whey obtained from acid coagulation is called acid whey and that obtained from rennet coagulation, sweet whey.

25

Liquid whey generally consists of the following: 88.7 % w/v water, 0.9 % w/v protein (mostly lactalbumin), 5.1 % w/v lactose, 0.3 % w/v fat and 5 % w/v minerals. The total solids content typically is in the range 5-10 % w/v. Large scale
30 drying techniques have in recent years been developed, which make the production of dry whey solids both technically possible and economically feasible. A large proportion of dried whey produced is still used as animal feed. Utilization of dried whey in food compositions for human consumption has

-2-

been limited because of functional deficiencies inherent in dry whey solids such as insolubility. In most industrial processes the whey protein is purified by advanced ultrafiltration, micro-filtration or ion-exchange techniques. This is followed by conventional spray-drying procedures. The whey protein thus obtained is not denatured and will form gels or coagulate when heated or acidified. Liquid egg white typically comprises 88.5 % w/v water and 9.8 % w/v ovalbumin, with the balance made up of minor amounts of fat, minerals and glucose. Spray-dried native egg white and whey protein are often difficult to dissolve in water, coagulate when heated and acidified and have poor emulsification properties.. Native whey and egg white do not denature when dried using conventional spray drying techniques : "although spray-dried products comes into contact with hot air, at no stage during the process does the product temperature become high enough to cause product denaturation" Spray drying handbook, Keith Masters, 5th edition. Publishers: Longman Scientific & Technical". Whole dry whey generally contains usually 12 % w/v by weight of protein.

It is an object of the present invention to avoid or minimize one or more of the above disadvantages.

25 It has now surprisingly been found that by carefully controlling the denaturation of albumin during pasteurization thereof, it is possible to obtain a fat replacement product which is safe and has very good processing characteristics, whilst being substantially free of coagulation or degradation 30 resulting from hydrolysis thereof.

The present invention provides a method for the manufacture of a fat replacement material suitable for use in the manufacture of food products, which method comprises the steps of:

-3-

- a) providing a substantially homogeneous aqueous fluid containing albumin and at least one stabilizer selected from a sugar and salt;
- b) subjecting said fluid to a controlled heat treatment at a temperature and for a period of time not less and not greater than that sufficient for obtaining from 50 to 100% denaturation of said albumin; and
- c) spray drying of the heat treated fluid.

10 Thus we have found that by carefully controlling the heat treatment, it is possible to obtain a degree of denaturation (loss of secondary and/or tertiary structure) of the albumin which makes it highly suitable for use in fat replacement, whilst at the same time avoiding the risk of coagulation
15 and/or hydrolysis which occur if heat treatment is allowed to continue for any significant period of time beyond that required to achieve 100 % denaturation. Preferably the thermal treatment conditions are selected so as to obtain from 55 to 90 % denaturation, advantageously from 60 to 80 %
20 denaturation. Desirably there is obtained at least 70 % denaturation.

The fat replacement materials provided by the present invention provide a number of significant advantages over
25 previously known materials. In general they have comparable or superior physical and processing qualities, whilst at the same time being considerably cheaper to produce. Thus, for example, whilst a current commercial process may take as long as 14 days to produce the material, the method of the present
30 invention can be completed within just one or two days using normal batch processing procedures. The excellent properties of the materials of the present invention include inter alia the following:

-4-

- Stability against heat and acid conditions. When dissolved in water in concentrations ranging from 0.1-70% w/v, thereby providing a protein concentration of up to 30% w/v, the onset of protein coagulation when heated, is substantially delayed and precipitation when acidified, substantially avoided. This is a significant improvement when compared to any spray-dried egg white or whey protein currently available in the food sector. The products can be used in pasteurized sauces, spreads (e.g. cheese spread) and innovative soft cheeses.
- 10 Excellent emulsifying capacity. The new materials can partially replace egg yolk in emulsions like mayonnaises and dressings, thereby lowering cholesterol content and reducing costs.
- Improved solubility in water at room temperature.
- 15 Other advantageous properties which may be mentioned include inter alia improved foaming capacity, improved water binding resulting in improved thickening power and emulsion stabilisation properties, and reduced allergenicity.
- 20 The fat replacement materials of the current invention closely resemble the functionality of sodium caseinate in food applications. Sodium caseinate obtained by alkali neutralization of casein has found broad utility in dairy products such as coffee whiteners, whipped toppings, frozen
- 25 desserts custards, processed cheese, sour creams, instant breakfasts, baby foods and the like. In compositions containing fat or oil and water, this ingredient serves to encapsulate the oil droplets and bind water, thus stabilizing the composition and prevents separation of oil from water. In
- 30 compositions where air is beaten into the mixture, sodium caseinate serves to further bind the air bubbles to the encapsulated oil, and thus stabilize the foam, i.e. the air, water, fat system. The denatured albumin of the fat replacement materials of the present invention can effectively

-5-

replace sodium caseinate in such products. The particular significance of this is that Na-caseinate is a very expensive raw material and the replacement thereof by the much more economically obtainable material of the present invention will lead to cost reduction of food products.

It will be appreciated that various different sets of conditions may be used to achieve a desired degree of denaturation with longer times being generally required at lower treatment temperatures and vice versa. The heat treatment conditions which can be safely used without coagulation of the albumin, will also depend on the nature and amount of stabilizer(s) used. At the same time it should also be borne in mind that certain stabilizers such as sugar and salt in particular, have other useful functions in fat replacers in relation to their final use in food products, and thus it may be preferred to use greater or lesser amounts of these than might otherwise be the optimum in relation to their stabilizing function, and/or greater or lesser amounts of different kinds of stabilizer for different product applications. Thus, for example, where the fat replacement material of the invention is intended for use in cakes and the like, then the stabilizer would generally include little or no salt and substantial amounts of sugar. Conversely in cheese spread applications, the stabilizer would contain little or no sugar, and relatively substantial amounts of salt.

Advantageously the stabilizer includes at least one food grade oil.

Preferably there is used in the process of the present invention a fluid comprising:
from 50 to 97 % w/v liquid albumin; and

-6-

from 3 to 50 % w/v of at least one stabilizer selected from salt, a sugar, and optionally an oil.

In general suitable amounts of the abovementioned individual 5 stabilizers, will be in the range of:

from 0 to 40 % w/v of salt;

from 0 to 30 % w/v of a sugar; and

from 0 to 10 % w/v of an oil.

10 Thus it will be understood that there may be used a stabilizer consisting of only a sugar or salt. We have found though, that when a sugar and salt are used together, there is obtained a synergistic effect on the stabilizing performance of the stabilizer component, and it is accordingly preferred 15 to use at least some sugar together with at least some salt.

In preferred forms of the present invention there are used fluid mixtures having the following compositions before spray drying, the albumin being in liquid form:

20 1. Egg white albumin based material

sugar 1-10 % w/v

salt 2-20 % w/v

oil 1-10 % w/v

albumin 60-90 % w/v

25 2. Whey albumin based material

sugar 0.1-10 % w/v

salt 2-20 % w/v

oil 1-10 % w/v

albumin 60-90 % w/v

30

Specific examples of the invention which may be mentioned use the following fluid mixture compositions, the albumin being in liquid form:

1. Egg white albumin based material

-7-

sugar 5 % w/v
salt 10 % w/v
oil 1 % w/v
albumin 84 % w/v

5 2. Whey albumin based material

sugar 5 % w/v
salt 10 % w/v
oil 1 % w/v
albumin 84 % w/v

10

In the above mixtures, the amounts of liquid albumin are based on normal unmodified (with respect to water content) forms thereof. Thus, for example, naturally occurring egg white and whey typically have a solids content of around 8 to 10 % w/v.

15 Nevertheless it would in principle also be possible to use liquid albumin with a somewhat reduced or somewhat increased water content, although this would generally be less convenient. In general the fluid mixture of liquid albumin and stabilizer would have a water content in the range from
20 0.5 to 40 % w/v, preferably from 10 to 30 % w/v. Moreover, as liquid mixtures with solids contents generally in the range from 15 to 35 % w/v can be readily spray dried, the solids content of typical liquid albumin + stabilizer mixtures used in the process of the present invention, will often be
25 suitable for spray drying without the need for any adjustment of the water content prior to spray drying.

As used herein salt normally indicates NaCl. It will nevertheless be appreciated that other physiologically salts
30 (e.g. KCl) could also be used. Various sugars, or mixtures, thereof may also be used, including, for example, fructose, glucose, sucrose, lactose, pectin, molasses, honey, dextrin, guar gum, locust bean gum or any water soluble starch, or any other sugar suitable for use in food products. Similarly

-8-

various animal () or vegetable oils suitable for use in food products may be used, including, for example, sunflower oil, olive oil, soya oil, liquefied butterfat, rape seed oil, etc.

5 Whilst whey and egg white are particularly convenient and abundant sources of albumin, various other albumins may also be used in accordance with the present invention. In general suitable albumins are hydrophilic globular proteins containing disulphide bonds and having a molecular weight of the order of
10 30-70 kilodaltons. Other suitable albumin sources include milk serum, soya protein, pea protein, and blood serum. It should also be noted that two or more different albumins may be used together.

15 Suitable conditions for the heat treatment may be readily determined by means of monitoring the degree of denaturation of the albumin. Various techniques are known in the art for measuring the degree of denaturation of albumin and other proteins. In one such method the denaturation degree is
20 determined by measuring the quantity of reactive SH-groups (N. Kitabake and E. Doi: Conformational changes of hen egg ovalbumin during foam formation detected by 5,5'-dithiobis(2-nitrobenzoic acid). J. Agric. Food Chem. (1987), 35 (953-975)).

25

In general we have found that suitable amounts of denaturation can be safely obtained by means of a thermal treatment step using a temperature of from 55 to 85 °C albeit that certain albumins such as ovalbumin prefer lower temperatures than
30 other albumins such as whey albumin. Thus in the case of ovalbumin there is preferably used a temperature of from 55 to 70 °C , whilst for whey albumin there is preferably used a temperature of from 65 to 80 °C. It will be appreciated that with higher temperatures there should generally be used a

-9-

shorter treatment period. Suitable treatment times would typically be from 2 to 10 minutes at from 70 to 80 °C, and from 10 to 30 minutes at lower temperatures.

5 Preferably the heat treatment is carried out under generally neutral pH, preferably in the range from 5 to 9. If desired, the mixture may be acidified after the heat treatment step, for example, to a pH in the range from 2 to 6. Suitable food grade acids which may be used to reduce the pH of the mixture
10 include acetic acid, conveniently in the form of vinegar.

The fat replacement materials of the present invention may be used in a wide variety of applications. Thus the products can be used as nutritive fat replacers in dairy products such as
15 coffee whiteners, whipped toppings, frozen desserts custards, processed cheese, sour creams, yoghurt, instant breakfasts, baby foods and the like. Thanks to their heat and acid stability the products can also be used in pasteurized sauces, soups and spreads (e.g. cheese spread) and innovative soft
20 cheeses, under pH conditions in the range from pH 2 to 8. Due to their excellent emulsifying capacity, the new products can also partially replace egg yolk in emulsions like mayonnaises and dressings, thereby lowering cholesterol content and reducing costs.

25

In general, the fat replacement materials of the invention will be reconstituted prior to mixing together with the other food product ingredients used in the preparation of the food product concerned, by mixing the material with water. In this
30 connection it will be appreciated that as liquid whey generally contains considerably less albumin than does egg white, then fat replacement materials of the invention based on the former, will generally be used in a more concentrated form when reconstituted (i.e. less water added to reconstitute

-10-

them), in order to obtain a given desired level of denatured albumin in the food product. Similarly, where liquid whey is used as the source of albumin, this may advantageously be concentrated in a preliminary step before use in the process of the present invention, for example by ultrafiltration, rotary evaporation, or any other convenient means known in the art. Typically the liquid whey would be concentrated around 10-fold.

10 The mixture of denatured liquid albumin and stabilizer is generally dried in an atomising type dryer, preferably so as to give a particle size of the order of 50 to 200 microns. The drying process effects drying of liquid by reducing or atomising the liquid feed stream containing dissolved solids into droplet form in the presence of a drying atmosphere. The atomising drier generally includes a main drying chamber, an atomiser, e.g. a spray nozzle, adapted to feed the material to be dried into the spray-drying atmosphere in the dryer chamber. In a conventional dryer, the inlet air stream is generally heated to effect drying. Typically there may be used an air temperature within the range from 168°C to 182°C. The corresponding outlet temperature range would typically be 110°C to 116°C. The temperature in the dryer is not critical provided that the temperature is high enough to effectively dry the products, yet insufficient to cause burning or browning. The parameters of the dryer as well as the conditions employed such as feed rate and residence time may be adjusted in generally known manner so as to avoid substantially burning or browning.

30

In spray drying of denatured egg white, the problem of browning of the powdered product, caused by the interaction of reducing sugars and amino acids, could arise. This problem may be generally avoided by limiting the temperature used in the

-11-

thermal treatment step preferably to below 70°C for example from 55°C to 70°C. Ovalbumin has a covalently bound sugar unit whereas whey albumins have none. Yet the tendency for browning in whey powders is less than in egg white, although lactose, which is a reducing sugar, is present in whey. The reason is that the covalently bound sugar in egg white has an open structure and is more reactive, whereas unbound sugar, such as lactose or glucose has a ring form in solution and is less reactive. This fact supports the assumption that the addition of the reducing sugar, glucose, to proteins in the current invention do not accelerate the browning reaction. In the conventional method for spray drying of egg white no oil is added. It is postulated that in the current innovative process, the proteins are denatured in controlled manner by heating under controlled conditions in the presence of sugar, salt and/or oil stabilizer, resulting in different secondary and tertiary structures than the native proteins. The denatured proteins are unfolded, the disulfide links are broken, and the hydrophobic areas are absorbed onto the oil-droplet surface. Where an oil stabilizer is included, the fluid mixture is desirably subjected to sufficient mixing or homogenisation so that an emulsion is formed which reduces the average oil droplet size. Such factors also contribute to counteract browning of egg white during and after spray drying.

In general, for spray drying purposes, the total solids content of the liquid mixture should be within the range of 15 to 35% and have a viscosity less than 125 cps (centipoise), as measured by, for example, a Brookfield disk spindle viscometer).

A small proportion of drying agent or a flow control agent such as tricalcium phosphate, dicalcium phosphate, kaolin,

-12-

diatomaceous earth, silica gel, calcium silica hydrate or mixtures thereof may advantageously be added to the fat replacement materials provided by the present invention in order to help maintain the free-flowing handling

5 characteristics of the materials and minimise any possible degradation thereof due to moisture absorption during storage etc.

Various other additives may also be included in the fat
10 replacement materials provided by the present invention.
Thus, for example, casein and/or other high molecular weight (biological) emulsifiers could be included, albeit in view of the excellent emulsifying and other properties of the materials provided by the process of the present invention,
15 there is normally little or no need for such additives.

Preferred forms of the dry powder fat replacement materials of the present invention typically have a composition of:

20 sugar	10-50 % w/v
salt	5-50 % w/v
oil	1-20 % w/v
albumin (50 to 100 % denatured and substantially non-coagulated and non-hydrolyzed)	10-80 % w/v

25

In a further aspect the present invention provides a fat replacement material comprising a spray dried powder comprising an intimate admixture of 1 part by weight of from 50 to 100 % denatured albumin, and from 3 to 100 parts by
30 weight of at least one stabilizer selected from a sugar and salt.

-13-

Further preferred features and advantages of the invention will appear from the following examples provided for the purposes of illustration.

5 Example 1 - Process for the preparation of Ovalbumin based Fat Replacement Material

A fluid albumin mixture was prepared by mixing together the following ingredients:

850 kg egg white - containing 5-6% w/v egg yolk

10 100kg sugar (cane or beet)

50kg salt

The egg mixture was stirred for 10 minutes at room temperature in a vacuumed container to prevent foaming.

The egg mixture was pasteurised on an industrial scale
15 pasteuriser (containing plate heat exchanger) at 63 degrees C for a holding time of 10 minutes.

The denaturation degree, as tested by determination of the quantity of reactive SH groups, should be at least 60% compared to the unpasteurised sample (0% denaturation). As a
20 reference level for 100% denaturation, the quantity of reactive SH-groups in a coagulated sample of the egg mixture was determined.

The pasteurisation holding time should be increased if the denaturation degree is below 60% and reduced if the
25 denaturation degree for the egg white mixture exceeds 80%. Finally the pasteurised (heat treated) egg mixture is then spray dried in a spray drier with a centrifugal cup spray nozzle. The inlet temperature should be around 170°C and the outlet at approximately 110°C.

30

Example 2 - Process for the preparation of mayonnaise
Standard (prior art) recipe

10 % w/v whole egg (4 % w/v yolk, 6 % w/v egg white)

10 % w/v sugar

-14-

1 % w/v salt
8 % w/v vinegar (10 % w/v acetic acid)
1 % w/v spices
70 % w/v oil

5

Modified (fat reduced) recipe

10 % w/v reconstituted spray dried egg mixture (3 % w/v egg powder obtained according to Example 1 +7 % w/v water)
9 % w/v sugar

10 0.5 % w/v salt

8 % w/v vinegar (10 % w/v acetic acid)
1 % w/v spices
40 % w/v oil
31.5 % w/v water

15

Preparation

Mix egg mixture, sugar, salt, water, spices and vinegar
Slowly add the oil while emulsifying (homogenising)

20 Properties of reduced fat mayonnaise compared to standard mayonnaise

It has similar viscosity and texture (mouthfeel)

It has similar storage stability (no water separation at the bottom of the jar)

25 Fat content is reduced by 30%

Cholesterol content is significantly reduced: 4% egg yolk in standard recipe reduced to 0.5%

Example 3 - Process for the preparation of Whey based Fat

30 **Replacement Material**

Liquid sweet whey is initially concentrated 10 fold using an evaporator at a maximum temperature of 50 degrees C.

A fluid albumin mixture was then prepared using the following ingredients:

-15-

900 kg concentrated liquid sweet whey (containing 9-10% whey protein)

50kg sugar

50kg salt

5

The mixture was then processed as follows:

Heat the whey mixture in a Stefan mixer while stirring to 75 degrees C. Hold the mixture at this temperature for 5 minutes, then cool to room temperature.

- 10 The denaturation degree, as tested by determination of the quantity of reactive SH groups, should be at least 70% compared to the unheated sample (0% denaturation). As control for 100% denaturation, the quantity of reactive SH-groups in a whey mixture sample heated at 75 for 30 minutes should be
- 15 determined.

The holding time at 75 degrees C should be increased if the denaturation degree is below 70%.

- Spray dry the pasteurised egg mixture in a spray drier with a centrifugal cup spray nozzle. The inlet temperature should be
- 20 around 170°C and the outlet at approximately 110°C.

Example 4 - Process for the preparation of mayonnaise

- The procedure of Example was followed using the fat
- 25 replacement material of Example 3 in place of that of Example 1, and similar results obtained.

-16-

CLAIMS

1. A method for the manufacture of a fat replacement material suitable for use in the manufacture of food products, which method comprises the steps of:
 - 5 a) providing a substantially homogeneous aqueous fluid containing albumin and at least one stabilizer selected from a sugar and salt;
 - b) subjecting said fluid to a controlled heat treatment at a temperature and for a period of time not less and not greater
10 than that sufficient for obtaining from 50 to 100% denaturation of said albumin; and
 - c) spray drying of the heat treated fluid.
2. An apparatus according to claim 1 wherein the albumin is
15 obtained from at least one of egg white, whey, milk serum, soya protein, pea protein, and blood serum.
3. An apparatus according to claim 2 wherein the albumin is used in the form of at least one of liquid egg white and whey.
20
4. An apparatus according to any one of claims 1 to 3 wherein in said heat treatment step said temperature and time period are selected so as to provide from 55 to 90 % denaturation.
- 25 5. An apparatus according to claim 4 wherein in said heat treatment step said temperature and time period are selected so as to provide 60 to 80 % denaturation.
6. An apparatus according to any one of claims 1 to 5 wherein
30 the stabilizer comprises a sugar and a salt.
7. An apparatus according to any one of claims 1 to 6 wherein the stabilizer includes an oil.

-17-

8. An apparatus according to claim 7 wherein is used at least one oil selected from sunflower oil, olive oil, soya oil, liquefied butterfat, and rape seed oil.
- 5 9. An apparatus according to any one of claims 1 to 8 wherein is used at least one sugar selected from fructose, glucose, sucrose, lactose, pectin, molasses, honey, dextrin, guar gum, locust bean gum or any water soluble starch, or any other sugar suitable for use in food products.
- 10 10. An apparatus according to any one of claims 1 to 9 wherein is used a fluid comprising:
from 50 to 97 % w/v liquid albumin; and
from 3 to 50 % w/v of said at least one stabilizer.
- 15 11. An apparatus according to any one of claims 1 to 10 wherein the stabilizer component in said fluid is constituted by:
from 0 to 40 % w/v of salt;
20 from 0 to 30 % w/v of a sugar; and
from 0 to 10 % w/v of an oil,
provided that the total amount of stabilizer component is not less than 3 % w/v.
- 25 12. An apparatus according to any one of claims 1 to 11 wherein said fluid consists essentially of:
sugar 1-10 % w/v
salt 2-20 % w/v
oil 1-10 % w/v
30 ovalbumin 60-90 % w/v.
13. An apparatus according to any one of claims 1 to 11 wherein said fluid consists essentially of:
sugar 0.1-10 % w/v

-18-

salt	2-20 % w/v
oil	1-10 % w/v
lactalbumin	60-90 % w/v

5 14. An apparatus according to any one of claims 1 to 13
wherein in said thermal treatment step there is used a
temperature of from 55 to 85 °C.

15 15. An apparatus according to claim 14 wherein in the case of
10 ovalbumin there is used a thermal treatment temperature of
from 55 to 70 °C.

16. An apparatus according to claim 14 wherein in the case of
lactalbumin there is used a thermal treatment temperature of
15 from 65 to 80 °C.

17. An apparatus according to any one of claims 1 to 14
wherein there is used a treatment time of from 2 to 10 minutes
at from 70 to 80 °C.

20

18. An apparatus according to any one of claims 1 to 14
wherein there is used a treatment time of from 10 to 30
minutes at from 55 to 70 °C.

25 19. An apparatus according to any one of claims 1 to 18
wherein the heat treatment is carried out at a substantially
neutral pH, in the range from 6 to 8.

20. A fat replacement material comprising a spray dried powder
30 comprising an intimate admixture of 1 part by weight of from
50 to 100 % denatured albumin, and from 3 to 100 parts by
weight of at least one stabilizer selected from a sugar and
salt.

-19-

21. A fat replacement material according to claim 20 wherein said albumin is from 55 to 95 % denatured.

22. A fat replacement material according to claim 20 or claim 5 21 wherein is included an oil stabilizer.

23. A fat replacement material according to any one of claims 20 to 22 wherein said albumin comprises at least one of lactalbumin and ovalbumin.

10

24. A food product containing a fat replacement material according to any one of claims 20 to 23.

INTERNATIONAL SEARCH REPORT

International Application No

PCT/GB 01/05648

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 A23C1/04 A23C21/00 A23L1/24 A23J1/08 A23J1/20
 A23J3/04 A23J3/08 A23L1/307

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 A23C A23L A23J

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data, PAJ

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP 0 579 328 A (CAMPINA MELKUNIE BV) 19 January 1994 (1994-01-19) page 2, line 29 -page 3, line 18; claims 1-11; examples 1-7	1-24
X	EP 1 042 960 A (KRAFT FOODS INC) 11 October 2000 (2000-10-11) paragraphs '0018!', '0019!', '0025!'-'0027!; claims 1-6; examples 1-6	1-11, 13, 14, 16-24
X	US 3 930 039 A (KUIPERS ARIE) 30 December 1975 (1975-12-30) claims 1-3; examples 1-3,5	1-3, 6-11, 13, 14, 16-19, 24
	--- -/--	

☒ Further documents are listed in the continuation of box C.☒ Patent family members are listed in annex.

* Special categories of cited documents:

- *A* document defining the general state of the art which is not considered to be of particular relevance
- *E* earlier document but published on or after the international filing date
- *L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- *O* document referring to an oral disclosure, use, exhibition or other means
- *P* document published prior to the international filing date but later than the priority date claimed

- *T* later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
- *X* document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
- *Y* document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
- *&* document member of the same patent family

Date of the actual completion of the international search

8 April 2002

Date of mailing of the international search report

17/04/2002

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
 NL - 2280 HV Rijswijk
 Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
 Fax: (+31-70) 340-3016

Authorized officer

Heirbaut, M

INTERNATIONAL SEARCH REPORT

International Application No

PCT/GB 01/05648

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP 0 779 035 A (SNOW BRAND MILK PROD CO LTD) 18 June 1997 (1997-06-18) page 3, line 32-37; claims 3,10; examples 1-5 page 4, line 2-4 ----	1-3, 6-11,14, 16,20-24
X	US 5 494 696 A (HOLST HANS H ET AL) 27 February 1996 (1996-02-27) column 3, line 17-25; claims 1,6,7,10,11,14,16 column 4, line 30-42 column 5, line 22-57; examples 1-5 ----	1-11,14, 16-19,24
X	EP 0 788 747 A (NESTLE SA) 13 August 1997 (1997-08-13) claims 2,4-6; examples 2-4 ----	24
X	US 5 350 590 A (MCCARTHY ANTHONY J ET AL) 27 September 1994 (1994-09-27) column 9, line 48-57; claims 1,7,8,22,26,41,45 column 11, line 1-18 column 12, line 1-25; example 1 ----	1-11,14, 16-19,24
X	EP 0 412 590 A (UNILEVER NV ;UNILEVER PLC (GB)) 13 February 1991 (1991-02-13) page 1, line 30-35; claims 1,5,6,14,17,24 page 2, line 1-4,10-24,50-58 ----	1-3, 6-11,14, 16-24
X	US 5 217 741 A (KAWACHI KIMIE ET AL) 8 June 1993 (1993-06-08) claims 1,2,8,13-20 ----	24
A	EP 0 619 075 A (GEN FOODS KRAFT R & D) 12 October 1994 (1994-10-12) the whole document -----	1-24

INTERNATIONAL SEARCH REPORT

 International Application No
 PCT/GB 01/05648

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
EP 0579328	A	19-01-1994	NL 9201264 A	01-02-1994
			AT 132704 T	15-01-1996
			CA 2100032 A1	15-01-1994
			DE 69301287 D1	22-02-1996
			DE 69301287 T2	18-07-1996
			DK 579328 T3	20-05-1996
			EP 0579328 A1	19-01-1994
			ES 2083820 T3	16-04-1996
			US 5462759 A	31-10-1995
EP 1042960	A	11-10-2000	US 6168819 B1	02-01-2001
			CA 2304319 A1	06-10-2000
			CN 1277807 A	27-12-2000
			EP 1042960 A2	11-10-2000
			JP 2001017079 A	23-01-2001
US 3930039	A	30-12-1975	DE 2138277 A1	08-02-1973
			AU 451606 B	15-08-1974
			AU 3352671 A	22-03-1973
			FR 2149039 A5	23-03-1973
			GB 1313085 A	11-04-1973
			JP 56001053 B	10-01-1981
			NL 7113312 A ,B,	01-02-1973
			NL 7215050 A	11-05-1973
			SE 384314 B	03-05-1976
EP 0779035	A	18-06-1997	AU 708893 B2	12-08-1999
			AU 4188296 A	05-02-1997
			EP 0779035 A1	18-06-1997
			FI 970921 A	07-04-1997
			JP 2966110 B2	25-10-1999
			NO 970974 A	30-04-1997
			NZ 297098 A	26-02-1998
			US 5902630 A	11-05-1999
			CA 2199124 A1	23-01-1997
			WO 9701964 A1	23-01-1997
US 5494696	A	27-02-1996	DE 4313014 A1	16-12-1993
			AT 146041 T	15-12-1996
			AU 666197 B2	01-02-1996
			AU 4064593 A	04-01-1994
			CA 2137913 A1	23-12-1993
			DE 59304753 D1	23-01-1997
			DK 644720 T3	13-10-1997
			WO 9325086 A1	23-12-1993
			EP 0644720 A1	29-03-1995
			ES 2098738 T3	01-05-1997
			GR 3022771 T3	30-06-1997
			JP 7507452 T	24-08-1995
			NZ 252136 A	26-10-1995
EP 0788747	A	13-08-1997	EP 0788747 A1	13-08-1997
			AU 732387 B2	26-04-2001
			AU 1253697 A	14-08-1997
			BR 9700900 A	12-01-1999
			CA 2197106 A1	09-08-1997
			CN 1159892 A	24-09-1997
			FI 970518 A	09-08-1997

INTERNATIONAL SEARCH REPORT

International Application No

PCT/GB 01/05648

Patent document cited in search report		Publication date	Patent family member(s)	Publication date
EP 0788747	A		JP 9215480 A NO 970254 A PL 318345 A1 US 5958498 A ZA 9700876 A	19-08-1997 11-08-1997 18-08-1997 28-09-1999 03-08-1998
US 5350590	A	27-09-1994	NONE	
EP 0412590	A	13-02-1991	AU 6025290 A CA 2022921 A1 EP 0412590 A1 IE 902852 A1 JP 3087148 A ZA 9006342 A	14-02-1991 11-02-1991 13-02-1991 27-02-1991 11-04-1991 29-04-1992
US 5217741	A	08-06-1993	JP 2529052 B2 JP 5064550 A	28-08-1996 19-03-1993
EP 0619075	A	12-10-1994	AT 148307 T AU 673579 B2 AU 5919094 A CA 2119117 A1 DE 69401604 D1 DE 69401604 T2 DK 619075 T3 EP 0619075 A1 ES 2097001 T3 NZ 260269 A US 5580592 A	15-02-1997 14-11-1996 13-10-1994 10-10-1994 13-03-1997 28-05-1997 30-06-1997 12-10-1994 16-03-1997 27-04-1995 03-12-1996